

<sup>16</sup> B The results shown in Table 2 demonstrate that the catalysts of the invention exhibit very high NO<sub>2</sub> decomposition performance even at temperatures below 300°C. On the other hand, with Comparative Example 1 which had Pt and Ba both present on the γ-alumina carrier, the NO<sub>2</sub> decomposition performance was slightly lower than that of the catalysts of the invention. The catalyst of Comparative Example 2 exhibited absolutely no NO<sub>2</sub> decomposition performance. The reason is believed to be its structure wherein no catalyst was carried on the filter.

Page 12, table 3, delete current table and insert therefor:

**Table 3 Comparison of particulate matter (PM) combustion rates**

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	Catalyst		PM combustion rate (mg/sec/L)	
	NO oxidation catalyst	NO <sub>2</sub> decomposition catalyst	200°C	250°C
Example 1	Pt/WO <sub>3</sub> /ZrO <sub>2</sub>	Pt/Ba/γ-alumina	0.04	0.12
Example 2	Pt/WO <sub>3</sub> /ZrO <sub>2</sub>	Fe/γ-alumina	0.04	0.11
Comp. Ex.1	Pt/Ba/γ-alumina		0.012	0.05
Comp. Ex.2	Upstream Pt/silica + monolith filter		0.002	0.006

Catalyst components: (2 g Pt + 0.1 g Rh)/1L filter

IN THE CLAIMS:

Please add new claims 7-10 as follows:

<sup>18</sup> B --7. A particulate matter combustion catalyst according to claim 1, wherein said NO oxidation catalyst and NO<sub>2</sub> decomposition catalyst are carried on a particulate matter filter.--

--8. A particulate matter combustion catalyst according to claim 2, wherein said NO oxidation catalyst and NO<sub>2</sub> decomposition catalyst are carried on a particulate matter filter.--